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## (54) Propylene polymer composition.

(57) The present invention relates to a propylene polymer composition comprising:  
65 to 95% by weight of a propylene homopolymer having (a) an intrinsic viscosity ( $[\eta_1]$ ) of 0.5 to 3.5 dl/g, (b) a xylene soluble content at ordinary temperature ( $X_s$ ) of not more than 3% by weight, and a difference ( $\Delta[\eta_1]$ ) between ( $[\eta_1]$ ) of xylene insoluble portion at the ordinary temperature and ( $[\eta_1]$ ) of

xylene soluble portion at the ordinary temperature of not more than 0.5 dl/g, (c) an isotactic pentad fraction (IP) falling within the range represented by the following equation:

$$IP \geq -0.624[\eta_1] + 97.5,$$

and (d) a crystallization temperature ( $T_c$ ) falling within the range represented by the following equation:

$$T_c \geq -2.33[\eta_1] + 116.0; \text{ and}$$

5 to 35% by weight of a propylene-ethylene random copolymer having (e) an intrinsic viscosity ( $[\eta_2]$ ) of less than 2.8 dl/g and (f) an ethylene content of 10 to 35% by weight.

Moldings obtained from the composition of the present invention are good in luster and high in both impact resistance and stiffness, and can find various applications as moldings well balanced in physical properties.

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## PROPYLENE POLYMER COMPOSITION

### BACKGROUND OF THE INVENTION

The present invention relates to a novel propylene polymer composition useful for production of moldings.

Isotactic polypropylene is used in a number of industrial fields because it is excellent in properties such as stiffness, heat resistance and surface luster and further is inexpensive. Isotactic polypropylene, however, is limited in its use because it is poor in impact strength and cannot be used in applications in which high mechanical impact is applied.

As methods for improving impact resistance of polypropylene, for example, (1) a method in which polypropylene and polyethylene or an ethylene-propylene elastomer are mechanically blended, and (2) a method for an impact resistant polypropylene composition usually called "block grade" in which propylene is first polymerized at the first step and at the second step, propylene and ethylene are copolymerized, are known.

Particularly, in the method (2), compositions prepared by uniformly mixing the homopolypropylene obtained at the first step with propylene-ethylene copolymers having various ethylene contents in various ratios have been proposed (Japanese Patent Publication No. 1886/1964).

These compositions, however, have a disadvantage in that excellent surface luster characteristic of polypropylene is reduced, although they are all improved in impact resistance. In recent years, with an extension of applications of impact resistant polypropylene, characteristics required for the polypropylene have been changing. That is, not only impact strength and stiffness, but also appearance characteristics, e.g., surface luster of molding, have becoming more important.

In recent years, a method in which at the first step, a small amount of ethylene is copolymerized for the purpose of improving physical properties of impact resistant polypropylene composition has been employed. In accordance with the above method, propylene and ethylene are copolymerized at the first step so that the ethylene content is 0.1 to 10% by weight, and the copolymer thus obtained is mixed with a propylene-ethylene copolymer obtained at the second step so that the ethylene content is not less than 70% by weight (see Japanese Patent Application Laid-Open No. 25291/1972). The method is intended to improve weld strength at the time of molding. However, such high impact strength that is expected as a block copolymer cannot be obtained. Furthermore the method has a disadvantage of decreasing stiff-

ness of molding.

### SUMMARY OF THE INVENTION

An object of the present invention is to provide a propylene polymer composition which provides moldings excellent in luster, stiffness and impact resistance and thus which can be used in a wide variety of applications as a general-purpose resin.

As a result of investigations to develop an impact resistant polypropylene composition well balanced in physical properties such as stiffness, impact strength and luster which is to be used in new applications, such as in production of car parts, home electric appliance parts, leisure parts and so forth and thus which can be used as a general-purpose resin, it has been found that the object can be attained by using a composition comprising polypropylene having specified physical properties and a propylene-ethylene copolymer having specified physical properties.

The present invention relates to a propylene polymer composition comprising:  
65 to 95% by weight of a propylene homopolymer having:

(a) an intrinsic viscosity,  $[\eta_1]$ , of 0.5 to 3.5 dl/g;

(b) a xylene soluble content at the ordinary temperature, Xs, of not more than 3% by weight, and a difference ( $\Delta[\eta_1]$ ) between an intrinsic viscosity ( $[\eta_1]$ ) of a xylene insoluble portion (at the ordinary temperature) and an intrinsic viscosity ( $[\eta_1]$ ) of a xylene soluble portion, i.e.,  $\Delta[\eta_1] = \text{intrinsic viscosity } ([\eta_1]) \text{ of insoluble portion} - \text{intrinsic viscosity } ([\eta_1]) \text{ of soluble portion}$  of not more than 0.5 dl/g;

(c) an isotactic pentad fraction, IP, falling within the range represented by the equation:  
$$IP \geq -0.624[\eta_1] + 97.5;$$

and (d) a crystallization temperature ( $T_c$ ) falling within the range represented by the following equation:

$$T_c \geq -2.33[\eta_1] + 116.0;$$

and

5 to 35% by weight of a propylene-ethylene random copolymer having:

(e) an intrinsic viscosity,  $[\eta_2]$ , of less than 2.8 dl/g; and

(f) an ethylene content of 10 to 35% by weight.

### DETAILED DESCRIPTION OF THE INVENTION

The propylene homopolymer to be used as the first component of the composition of the present invention is a propylene homopolymer characterized by the following requirements (a) to (d).

(a) The intrinsic viscosity,  $[\eta]$ , of the propylene homopolymer is 0.5 to 3.5 dl/g, preferably 1 to 3 dl/g, and more preferably 1.1 to 2.8 dl/g. If the intrinsic viscosity is more than 3.5 dl/g, fluidity at the time of melting is low. On the other hand, if it is less than 0.5 dl/g, the strength of the molding is decreased.

(b) The xylene soluble content at the ordinary temperature ( $X_s$ ) of the propylene homopolymer is not more than 3% by weight, preferably 2 to 0.1% by weight, and more preferably 1.5 to 0.2% by weight.

The xylene soluble content at ordinary temperature as used herein is a value as measured by the following method: (i)  $5 \pm 0.5$  g of a sample is completely dissolved in 700 ml of p-xylene, (ii) the resulting solution is cooled to ordinary temperature, (iii) the solution is filtered, and methanol is added to the separated solution to precipitate, iv) the filtration is again performed, and (v) the solids portion is dried at  $100^\circ\text{C}$  for 4 hours and weighed.

If the xylene solution content at ordinary temperature of the propylene homopolymer is more than 3% by weight, all stiffness, heat resistance and hardness drop.

In the propylene homopolymer of the present invention,  $\Delta[\eta]$  (=intrinsic viscosity  $[\eta]$  of xylene insoluble (ordinary temperature) portion - intrinsic viscosity  $[\eta]$  of xylene soluble (ordinary temperature) portion) is not more than 0.5 dl/g, preferably 0.4 to 0.1 dl/g. If  $\Delta[\eta]$  is more than 0.5 dl/g, both stiffness and heat resistance of the composition of the present invention are decreased.

The above intrinsic viscosity is measured in a tetralin solution at a temperature of  $135^\circ\text{C}$ .

(c) The isotactic pentad fraction (IP) of the propylene homopolymer of the present invention is in the range represented by the equation:

$$\text{IP} \geq -0.624[\eta] + 97.5,$$

specially

$$\text{IP} \geq -0.624[\eta] + 98.0.$$

If the isotactic pentad fraction is outside the above specified range, stiffness and heat resistance are decreased.

The isotactic pentad fraction as used herein means an isotactic fraction in the pentad unit as contained in the polypropylene chain as measured by the method disclosed in Macromolecules, 6 925 (1973) by A. Zambelli et al., i.e., the method using  $^{13}\text{C}$ -NMR. In other words, the isotactic pentad fraction is a fraction of propylene monomer units existing in the center of the chain in which five propylene monomer units are continuously linked together in the meso bond. Assignment of peaks was

made by the method described in Macromolecules, 8 687 (1975).

More specifically, the isotactic pentad unit is measured as an intensity fraction of mmmm peak in all absorption peaks in the methyl carbon region of  $^{13}\text{C}$ -NMR spectrum.

The value of the isotactic pentad fraction in the propylene homopolymer of the present invention is a value of the crystalline polypropylene obtained itself, but not that of the polymer after extraction, fractionation and so forth.

(d) The crystallization temperature  $T_c$  of the propylene homopolymer is within the range represented by the equation:

$$T_c \geq -2.33[\eta] + 116.0,$$

specifically

$$T_c \geq -2.33[\eta] + 117.0.$$

In the present invention, the crystallization temperature  $T_c$  was measured by the following method. That is, 8 mg of a sample was raised in temperature from  $50^\circ\text{C}$  to  $220^\circ\text{C}$  at a temperature raising speed of  $320^\circ\text{C}/\text{min}$  by the use of a differential scanning calorimeter and then maintained at that temperature for 10 minutes, and lowered in temperature to  $50^\circ\text{C}$  at a temperature lowering speed of  $10^\circ\text{C}/\text{min}$ .

In production of the propylene homopolymer as the first component of the composition of the present invention, it is desirable to use a stereoregularity polymerization catalyst, particularly a catalyst having a large stereoregularity tendency.

As such catalysts, for example, a catalyst containing (i) a reaction product of a magnesium compound and a titanium compound, (ii) an organometallic compound, and (iii) an electron donating compound as a component can be used.

As the reaction product of a magnesium compound and a titanium compound (i), a product obtained by contacting magnesium dialkoxide represented by the general formula:

$\text{Mg}(\text{OR}^1)_2$  (wherein  $\text{R}^1$  is an alkyl group having 1 to 20 carbon atoms) with an electron donating compound and if necessary, further with a halogenation agent, and then reacting with a halogen-containing titanium compound represented by the general formula:  $\text{Ti}(\text{OR}^2)_n\text{X}^{1-4-n}$  (wherein  $n$  is 0 to less than 4,  $\text{X}^1$  is a halogen atom, and  $\text{R}^2$  is an alkyl group having 1 to 20 carbon atoms) is preferably used.

As the organometallic compound (ii), organometallic compounds of aluminum, lithium, zinc and the like can be used. In particular, as the organoaluminum compound, an alkyl-aluminum compound represented by the general formula:

$\text{AlR}^3_m\text{X}^{2-3-m}$  (wherein  $\text{R}^3$  is an alkyl group having 1 to 20 carbon atoms,  $\text{X}^2$  is a halogen atom, and  $m$  is 0 to not more than 3) is preferably used.

As the electron donating compound (iii), organic compounds containing oxygen, nitrogen,

phosphorus, sulfur or the like are usually used.

More specifically, esters such as aromatic carboxylic acid esters, oxygen-containing silicon compounds such as diphenyldialkoxysilane, amines, amides, ketones, nitriles, phosphines, phosphoramides, esters, thioethers, thioesters, acid anhydrides, acid halides, organic acids and the like can be used.

In preparation of the reaction product of a magnesium compound and a titanium compound (i), magnesium dialkoxide and if necessary 0.01 to 10 mol of a halogenation agent are added, and an electron donating compound is added in an amount of 0.01 to 10 mol per mol of magnesium and a halogen-containing titanium compound is added in an amount of 1 to 50 mol per mol of magnesium, and they are reacted at a temperature of 0 to 200°C for a time of 5 minutes to 10 hours. In this case, the reaction is preferably carried out repeatedly twice or more times. The electron donating compound is chosen from the compounds listed as the electron donating compound (iii).

In preparation of the catalyst, if necessary, an inert solvent, e.g., hydrocarbons, can be used.

By polymerizing propylene by the use of the magnesium compound/titanium compound reaction product (i) (solid component) which has been treated with the organometallic compound (ii) and the electron donating compound (iii) under suitable conditions, a high stereoregularity propylene homopolymer can be obtained.

In this case, as the propylene starting material, high purity propylene is preferably used to obtain the propylene homopolymer of the present invention.

Polymerization method and polymerization conditions are not critical. Polymerization can be carried out, continuously or batchwise, by solution polymerization, suspension polymerization, gas phase polymerization and so forth.

In the case of the solution polymerization, the catalyst is used in such an amount that the concentration of the above solid component (calculated as a titanium atom) is from 0.001 to 1 mmol/l.

The organometallic compound (ii) to be used as a catalyst component for production of the propylene homopolymer to be used in the present invention can be used in the range of 1 to 1,000 mol per mol of a titanium atom.

The electron donating compound to be used as the component (iii) of the catalyst (which is added at the time of polymerization) can be used in an amount of 0.01 to 200 mol per mol of a titanium atom.

In connection with polymerization conditions, the polymerization can be carried out at a pressure of from atmospheric pressure to 50 kg/cm<sup>2</sup> and a temperature of from 30 to 200°C.

Controlling the molecular weight can be carried out by known techniques utilizing hydrogen or a catalyst composition.

The propylene homopolymer to be used in the composition of the present invention can be produced by a method as described above, that is, a known propylene polymerization method using a high stereoregularity catalyst, e.g., a method as described in, for example, Japanese Patent Application Laid-Open Nos. 63310/1982 and 146905/1988, more specifically by applying gas polymerization and so forth under conditions which have been determined taking into consideration the characteristics required for the polymer of the present invention (requirements (a) to (d)).

The propylene polymer composition of the present invention comprises a composition containing the propylene homopolymer as obtained above and a propylene-ethylene random copolymer as the second component.

It is necessary for the propylene-ethylene random copolymer to have an intrinsic viscosity of less than 2.8 dl/g, preferably 1 to 2.6 dl/g and more preferably 1.2 to 2.6 dl/g, and an ethylene content of 10 to 35% by weight, preferably 12 to 28% by weight. If the intrinsic viscosity is 2.8 dl/g or more, luster is decreased. If the ethylene content is less than 10% by weight, impact resistance is decreased. On the other hand, if it is more than 35% by weight, luster is decreased.

The propylene-ethylene random copolymer to be used as the second component in the present invention can be produced by copolymerizing propylene and ethylene by the use of the similar catalyst as the stereoregularity polymerization catalyst used in production of the propylene homopolymer as the first component under the similar polymerization conditions as in production of the propylene homopolymer as the first component.

The propylene polymer composition to be used in the composition of the present invention can be obtained by compounding the first and second components previously prepared, in a predetermined ratio, and can be efficiently produced, for example, by blending in a polymerization vessel by the two stage polymerization method.

In the first place, in the first stage polymerization vessel, the propylene homopolymer as the first component is produced by the above method. Then, in the second stage polymerization vessel, ethylene and propylene are copolymerized in the presence of the propylene homopolymer obtained at the first stage in such a manner that the intrinsic viscosity is within the above specified range, and the propylene homopolymer at the first stage (the first component) constitutes 65 to 95% by weight, preferably 70 to 93% by weight of the total polymer and the propylene-ethylene random copolymer

at the second stage (the second component) constitutes 5 to 35% by weight, preferably 7 to 30% by weight of the total polymer.

The composition thus obtained can be used as a molding material by compounding various additives such as an antioxidant by the usual method and then pelletizing.

Moldings obtained from the propylene polymer composition of the present invention are good in luster and high in both impact resistance and stiffness, and can find various applications as moldings well balanced in physical properties.

The present invention is described in greater detail with reference to the following examples.

#### EXAMPLE 1

##### (1) Preparation of Solid Catalyst Component

In a 4-liter glass container the atmosphere of which had been replaced with argon, 40 g of diethoxymagnesium, 600 ml of n-heptane and 40 mmol of di-n-butyl phthalate were placed, and they were then stirred at room temperature for 30 minutes. Then, 90 mmol of silicon tetrachloride was added to the solution as obtained above and stirred for one hour, and then 10 mol of titanium tetrachloride was added and stirred at 110°C for 2 hours.

The supernatant liquid was separated. After washing with hot n-heptane, 10 mol of titanium tetrachloride was added and stirred at 110°C for 2 hours. By thoroughly washing with n-heptane, a solid catalyst component was obtained.

The catalyst contained 2.2% by weight of Ti.

##### (2) Polymerization

In a 5-liter autoclave, after thoroughly replacing the atmosphere with nitrogen gas, 20 g of polypropylene which had been dried was placed. Then, 2.0 mmol of triethylaluminum, 0.1 mmol of diphenyldimethoxysilane and 0.01 mg (as titanium atom) of the above solid catalyst component were placed in the autoclave. Hydrogen and propylene were introduced, and the temperature and the pressure were increased to 70°C and 28 kg/cm<sup>2</sup>, respectively. Under these conditions, polymerization was carried out for two hours.

After the polymerization at the first stage was completed, degassing was once conducted. Then, a mixed gas of ethylene and propylene, and hydrogen were introduced. While maintaining the pressure at a mixed gas pressure of 18 kg/cm<sup>2</sup>, the second stage polymerization was carried out at 55°C for two hours.

After the completion of the second stage polymerization, unreacted gases were removed to obtain a propylene polymer composition shown in Table 1. To the propylene polymer thus obtained, conventionally known additives were added and mixed, and the resulting mixture was pelletized by the use of an extruder.

#### EXAMPLES 2 TO 4, AND COMPARATIVE EXAMPLES 1 TO 3

In Example 1, conditions for the first stage polymerization and/or conditions for the second stage polymerization were changed to obtain propylene polymer compositions shown in Table 1.

#### COMPARATIVE EXAMPLE 4

##### (1) Preparation of Solid Catalyst Component

In a 500-milliliter four-necked flask, 150 ml of dry n-heptane and 11.4 g (100 mmol) of magnesium diethoxide were placed, and at room temperature 1.45 ml (15 mmol) of carbon tetrachloride and 1.85 ml (6.2 mmol) of tetra-1-propoxytitanium were added.

The temperature was raised to 60°C, and the reaction was carried out for 2 hours.

The reaction product thus obtained was washed twice with 200 ml of dry n-heptane by the decantation method at room temperature. Then, 100 ml of dry n-heptane and 4.1 ml (23 mmol) of n-butyl benzoate were added, and then 110 ml (1,000 mmol) of titanium tetrachloride was dropped. The reaction was carried out at 108°C for two hours. At a temperature of 80 to 85°C, the supernatant liquid was withdrawn. Then, 200 ml of dry n-heptane was further added. The resulting mixture was stirred, allowed to stand, and the supernatant liquid was withdrawn. This procedure was repeated four times. Then, washing was performed twice at room temperature to obtain a solid catalyst component. The amount of titanium deposited as determined by the colorimetric method was 30 mg-Ti/g-solid catalyst component.

##### (2) Polymerization

A propylene polymer composition shown in Table 1 was obtained in the same manner as in Example 1 except that the above solid catalyst component was used as the solid catalyst component.

Moldings of the above compositions were mea-

sured for luster, impact strength and stiffness (modulus in flexure). The results are shown in Table 1.

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Table 1

	Example				Comparative Example			
	1	2	3	4	1	2	3	4
Propylene Homopolymer								
$[\eta]$ (dl/g)	1.1	1.4	1.7	2.6	1.4	1.3	1.3	1.6
Xylene Soluble Content at Ordinary Temperature (wt%)	1.3	1.0	0.7	0.5	1.0	1.1	1.1	4.0
$\Delta[\eta]$	0.3	0.2	0.2	0.3	0.2	0.3	0.3	0.7
IP	97.5	97.1	96.9	96.5	97.1	97.3	97.3	95.6
$-0.624[\eta] + 97.5$	96.8	96.6	96.4	95.9	96.6	96.7	96.7	96.5
Tc	118.3	115.8	115.2	111.4	115.8	116.3	116.3	107.4
$-2.33[\eta] + 116.0$	113.4	112.7	112.0	110.0	112.7	113.0	113.0	112.3
Amount of Polymer (wt%)	75	86	82	92	86	84	63	82
Propylene-Ethylene Random Copolymer								
$[\eta]$ (dl/g)	1.9	2.3	2.6	2.0	2.1	5.8	2.4	2.4
Ethylene Content (wt%)	21	25	15	24	58	25	26	23
Amount of Polymer (wt%)	25	14	18	8	14	16	37	18
Modulus in Flexure *1 (kg/cm <sup>2</sup> )	13100	14000	14100	14300	14100	14700	10800	12700
Izod Impact Strength *2 (-20°C) (kg·cm/cm)	4.5	2.4	2.1	2.1	2.7	2.3	5.9	2.2
Luster *3 (%)	90	93	92	94	65	71	54	87

\*1 Modulus in Flexure: Measured according to JIS K7203

\*2 Izod Impact Strength: Measured according to JIS K7110 (notched)

\*3 Luster: Measured according to JIS K7105

## Claims

1. A propylene polymer composition comprising:

65 to 95% by weight of a propylene homopolymer having (a) an intrinsic viscosity ( $[\eta_1]$ ) of 0.5 to 3.5 dl/g, (b) a xylene soluble content at ordinary temperature ( $X_s$ ) of not more than 3% by weight, and a difference ( $\Delta[\eta_1]$ ) between an intrinsic viscosity ( $[\eta_1]$ ) of xylene insoluble portion at the ordinary temperature and an intrinsic viscosity ( $[\eta_1]$ ) of xylene soluble portion at the ordinary temperature of not more than 0.5 dl/g, (c) an isotactic pentad fraction (IP) falling within the range represented by the following equation:

$$IP \geq -0.624[\eta_1] + 97.5,$$

and (d) a crystallization temperature ( $T_c$ ) falling within the range represented by the following equation:

$$T_c \geq -2.33[\eta_1] + 116.0; \text{ and}$$

5 to 35% by weight of a propylene-ethylene random copolymer having (e) an intrinsic viscosity ( $[\eta_2]$ ) of less than 2.8 dl/g and (f) an ethylene content of 10 to 35% by weight.

2. The composition as claimed in Claim 1, wherein the intrinsic viscosity  $[\eta_1]$  of the propylene homopolymer is 1 to 3 dl/g.

3. The composition as claimed in Claim 1, wherein the xylene soluble content at the ordinary temperature ( $X_s$ ) of the propylene homopolymer is 2 to 0.1% by weight.

4. The composition as claimed in Claim 1, wherein the difference ( $\Delta[\eta_1]$ ) between the intrinsic viscosity ( $[\eta_1]$ ) of xylene insoluble portion at the ordinary temperature and the intrinsic viscosity ( $[\eta_1]$ ) of xylene soluble portion at the ordinary temperature is 0.4 to 0.1 dl/g.

5. The composition as claimed in Claim 1, wherein the isotactic pentad fraction (IP) is in the range represented by the following equation:

$$IP \geq -0.624[\eta_1] + 98.0.$$

6. The composition as claimed in Claim 1, wherein the crystallization temperature ( $T_c$ ) is in the range represented by the following equation:

$$T_c \geq -2.33[\eta_1] + 117.0.$$

7. The composition as claimed in Claim 1, wherein the intrinsic viscosity ( $[\eta_2]$ ) of the propylene-ethylene random copolymer is 1 to 2.6 dl/g.

8. The composition as claimed in Claim 1, wherein the ethylene content of the propylene-ethylene copolymer is 12 to 28% by weight.

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(54) **Propylene polymer composition.**

(57) The present invention relates to a propylene polymer composition comprising:  
65 to 95% by weight of a propylene homopolymer having (a) an intrinsic viscosity ( $[\eta_1]$ ) of 0.5 to 3.5 dl/g, (b) a xylene soluble content at ordinary temperature (Xs) of not more than 3% by weight, and a difference ( $\Delta[\eta_1]$ ) between ( $[\eta_1]$ ) of xylene insoluble portion at the ordinary temperature and ( $[\eta_1]$ ) of xylene soluble portion at the ordinary temperature of not more than 0.5 dl/g, (c) an isotactic pentad fraction (IP) falling within the range represented by the following equation:

$$IP \geq -0.624[\eta_1] + 97.5,$$

and (d) a crystallization temperature ( $T_c$ ) falling within the range represented by the following equation:

$$T_c \geq -2.33[\eta_1] + 116.0; \text{ and}$$

5 to 35% by weight of a propylene-ethylene random copolymer having (e) an intrinsic viscosity ( $[\eta_2]$ ) of less than 2.8 dl/g and (f) an ethylene content of 10 to 35% by weight.

Moldings obtained from the composition of the

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## EUROPEAN SEARCH REPORT

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DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
X	EP-A-0 135 834 (HOECHST) * page 15, line 26 - line 37 ** page 14, line 20 - line 23 ** page 13, last paragraph ** page 10, line 26 - line 31 ** page 11, line 21 - line 27 ** page 16, line 10 - line 19 * - - -	1-8	C 08 L 23/16 C 08 L 23/12 C 08 F 297/08 // (C 08 L 23/12 C 08 L C 08 L 23:16 )
X	US-A-3 487 128 (M.OKAZAKI ET AL) * column 2, line 30 - line 62 ** column 3, line 5 - line 19 ** column 3, line 63 - column 4, line 7; table 1 * - - -	1-8	
X	US-A-4 211 690 (H.ASANO ET AL) * column 1, line 45 - line 57 ** column 2, line 4 - line 33 * - - -	1-8	
A	US-A-4 547 552 (A. TOYOTA ET AL) * column 3, line 13 - line 26 ** column 4, line 62 - line 66 ** column 8, line 58 - column 9, line 2 ** column 9, line 57 - column 10, line 16 ** column 10, line 32 - line 49 * - - - - -	1-8	
			TECHNICAL FIELDS SEARCHED (Int. Cl.5)
			C 08 L C 08 F
The present search report has been drawn up for all claims			
Place of search		Date of completion of search	Examiner
The Hague		19 November 91	SCHMIDT H.R.
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